

02/18/00  
JC551 U.S. PTO

02-22-00

PATENT APPLICATION

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

IN RE APPLICATION OF:

ATTORNEY'S DOCKET NUM

Andrew Eades and Jeffrey Penno

1473-991365

JC551 U.S. PTO  
09/5056780  
02/18/00

ENTITLED

"BUOYANT MEDIA FLOTATION"

To the Application Branch  
Assistant Commissioner for Patents  
Washington, D.C. 20231

EXPRESS MAIL CERTIFICATE

"Express Mail" Label Number EL314743307US

Date of Deposit February 18, 2000

I hereby certify that the following attached paper or fee

SPECIFICATION (7 pp.); CLAIMS (3 pp., 17 claims); ABSTRACT (1 p.); DRAWINGS (3 sheets); PATENT APPLICATION TRANSMITTAL LETTER (1 p., original and two (2) copies); DECLARATION AND POWER OF ATTORNEY (2 pp.); ASSIGNMENT (1 p.); RECORDATION FORM COVER SHEET (1 p.); POSTCARD AND CHECKS IN THE AMOUNTS OF \$690.00 AND \$40.00

is being deposited with the United States Postal Service "Express Mail Post Office to Addressee" service under 37 C.F.R. §1.10 on the date indicated above and is addressed to the Assistant Commissioner for Patents, Washington, D.C. 20231.

Michelle Pichora  
(Typed name of person mailing paper or fee)

Michelle Pichora  
(Signature of person mailing paper or fee)

**CERTIFICATE OF EXPRESS MAILING**

I hereby certify that this correspondence is being deposited with the United States Postal Service by Express Mail No. EH655258011US in an envelope address to the Assistant Commissioner for Patents, Washington, DC 20231 on February 18, 2000.

Signed: Patrick L. Pot

Dated: 2/18/00

**BUOYANT MEDIA FLOTATION**  
**BACKGROUND OF THE INVENTION**

1. Field of the Invention

5 The present invention relates to treatment systems for clarification of a fluid stream and, more particularly, to buoyant media introduced into the flow to induce a rising force on particles to be removed from the fluid.

10 2. Background of the Invention

Technologies for the separation of components of a fluid stream on the basis of density are well known in the art. The simplest systems rely on differences in densities alone to accomplish this separation, with heavier components settling, in the absence of agitation, to the bottom of the fluid for removal.

15 For small particles, the time required for the unassisted settling process can be unacceptably long. Stokes' Law predicts that spherical particles suspended in a fluid medium settle at a rate proportional to the second power of the particle diameter. Thus, large particles will settle much faster than smaller ones. To increase the rate of settling, coagulants can be used. A coagulant is a substance that produces a loosely-massed precipitate. As the precipitate forms, it entraps solid particles contained in the fluid. Aluminum sulfate and ferric sulfate are among the materials used in the art as coagulants.

20 30 Particles in solution often have a net surface charge. As a result, they tend to repel each other and resist the formation of agglomerates. Coagulation is the process whereby these repulsive charges are neutralized. After charge neutralization, the particles begin to collect into larger aggregates. This agglomeration process is known as flocculation; the resulting aggregate is known as a floc. Flocculant aids are thus effective as solid-liquid separating agents. Flocculant aids are typically synthetic water soluble polymers based on acrylamide. There are some natural occurring polymers, such as chitosan, that can be used for this purpose.

Entrainment can be used in conjunction with flocculation to expedite the separation process. For example, grains of sand can be introduced to the fluid to be treated. The floc that forms entraps the grains of sand, and the density of the floc is increased as is its settling speed. Alternatively, bubbles may be generated as the floc is formed, and their entrainment produces a floc that rises to the surface of the fluid rather than settling to the bottom. However, additional equipment and operating expenses are required to generate the bubbles. Other settling media may be selected on the basis of specific gravity, particle size, surface properties, or chemical properties. Increasing the concentration of these settling media improves the efficiency of the flocculation process, because more particle collisions result and the size of the resulting agglomerated particles increases more rapidly. Also, the settling capacity of the system increases with concentration. However, increasing the concentration of entrained materials increases the cost of the separation process, and increases the volume of the waste materials produced. For settling media with specialized properties, these cost constraints can be significant.

Solids separation processes employing settling inherently require energy in the flocculation stage, produce large volumes of sludge, produce effluent with small, difficult to settle particles, and require large, complex process vessels. These characteristics lead to increased costs. Accordingly, a need exists to reduce the costs associated with solids separation in high rate fluid clarification systems.

#### SUMMARY OF THE INVENTION

In order to meet this need, the present invention is a clarification system for fluids, in which particles are separated from the fluid by flotation and in which a buoyant media inducing the flotation is recycled. Buoyant media separation processes according to the invention offer a number of advantages over settling media processes

according to the invention. Less energy is required in the flocculation stage in a buoyant media separation process. The volume of sludge produced is lower, and the sludge solids concentration is higher; no further sludge concentration is required. Also, process vessel depth is substantially less for buoyant media separation processes, and process vessel construction is simpler and more economical.

Fluid to be treated passes into a mixing chamber in which it is mixed rapidly with coagulants and flocculants. The resulting mixture then passes into a flocculation chamber in which the buoyant media are added and mixed and in which the flocculation process produces agglomerated particles. The product of the flocculation chamber passes into a flotation chamber. The flotation chamber is configured so that the removal of clarified fluid draws the fluid entering the chamber upward, hastening the generation of a sludge layer containing separated particles and buoyant media at the top of the chamber.

Optionally, the flotation chamber can be equipped with a flotation assistance device, such as dissolved air flotation, diffused air, or froth flotation system, to further hasten the flow of separated particles and buoyant media upward. In addition, lamella plates, tubes or other coalescing surfaces can be added to the flotation chamber to improve the separation of the buoyant flocs. Submerged membrane systems can be provided in the separation tank to remove the need for downstream filtration systems.

The clarified fluid obtained from the separation of sludge is removed from the bottom of the flotation chamber, and is optionally filtered. The sludge layer is removed from the top of the flotation chamber by any of a number of methods of removal well known in the art, such as a mechanical skimmer or by hydraulic desludging. The sludge layer then passes into a buoyant media recovery unit, wherein the buoyant media are separated from the

5 sludge stream. The sludge stream is disposed of and the buoyant media are recycled into the flocculation chamber. The buoyant media recovery unit can make use of various types of devices to effect the separation, such as a centrifugal separator, centrifugal screener, cross-flow sieve, or vibratory screen separator. Alternately, the flocs can be subjected to shearing forces to separate the media from the waste particles, and the two phases are then allowed to separate.

10 **BRIEF DESCRIPTION OF THE DRAWING**

Fig. 1 is a schematic diagram of components and the pattern of flow of the clarifier device of the present invention.

15 Fig. 2 is a schematic diagram of a flotation chamber of the present invention, including lamella plates.

Fig. 3 is a schematic diagram of a flotation chamber of the present invention, including tubes.

20 Fig. 4 is a schematic diagram of a flotation chamber of the present invention, including an immersed membrane module.

**DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENT**

25 The high rate clarification system of this invention makes use of high concentrations of particles of a buoyant media. The high concentrations improve the efficiency of flocculation and enable the system to produce a high rate of flotation.

30 Referring to Fig. 1, fluid to be treated flows into a mixing chamber 10. A coagulant is added to the fluid in this chamber 10. The coagulants are typically metal salts, such as aluminum sulfate, ferric sulfate, or PACL, or can be any of the coagulant-type polymers currently offered by chemical suppliers. The amount of coagulant needed depends on factors, such as the concentration of solids to be removed from the fluid, but is typically in the range of 5 and 180 milligrams per liter of fluid.

After coagulant is added, the resulting mixture passes through a flocculation chamber feed line 14 into a flocculation chamber 20. In the flocculation process, aggregate suspended particles grow in size as they combine. 5 Buoyant media and a flocculant aid are added to the fluid mixture in chamber 20. A flocculant is added to chamber 20 with the buoyant media. Typical flocculants for this application are synthetic water soluble polymers based on acrylamide. There are also some naturally occurring 10 polymers that can be used such as chitosan. The amount of flocculant needed depends on factors, such as the concentration of solids to be removed from the fluid, but is typically in the range of 0.1 to 1.0 milligrams per liter of fluid. In the flocculation process, aggregate suspended particles grow in size as they combine. The 15 buoyant media may be finely divided solids, but may also be solids that have been foamed or otherwise provided with internal voids. The buoyant media may include a plastic powder which has a specific gravity less than 1.0. The plastic can be, for example, polypropylene or polyethylene, but there are various other lightweight materials that can be used. Particle size for the buoyant media may be in the 20 range of 10 to 500 microns, preferably in the range of 30 to 250 microns. The media will typically be added at a 25 rate of 0.1 to 5 grams per liter of fluid mixture.

The fluid mixture, containing coagulants, flocculants, buoyant media, and the solids to be separated, then passes through a flotation chamber feed line 24, into a flotation chamber 30. Flotation chamber 30 is configured 30 so that entering fluid is directed upward, expediting the flotation process. A baffle 32 is an example of a structure directing entering fluid upward. The action of the buoyant media, in conjunction with the coagulant and flocculant, result in the formation of a thick sludge layer 34 at the top of flotation chamber 30. The sludge layer 34 is separated from the flotation chamber 30 into a sludge 35 hopper 36. The separation can be effected by a chain-and-

flight or reciprocating skimmer or other sludge removal device. Sludge can also be removed from the chamber 30 by hydraulic desludging. A clarified fluid 38 is formed by the removal of coagulant and flocculant from the entering fluid by the buoyant media. Optionally, a flotation assistance device 40 can be used to further hasten the flow of separated particles and buoyant media upward. Flotation assistance device 40 may be a dissolved air flotation (DAF) system or DAF pump, or dispersed air system or blower. The output from flotation assistance device 40 enters flotation chamber 30 through a flotation assistance line 42.

Clarified fluid 38 is withdrawn from flotation chamber 30 through a clarified fluid withdrawal line 44 or other process outlet. Lamella plates 45, tubes 45' or an immersed membrane module 45" can be added to the flotation cell to hasten the separation process as shown in Fig. 2, Fig. 3 and Fig. 4. Optionally, a portion of the clarified fluid 38 can be recycled through a clarified fluid recycling line 46 to flotation assistance device 40.

The sludge layer 34 is removed from sludge tank 36 through a sludge line 48 to a buoyant media recovery unit 50. Buoyant media recovery unit 50 may make use of a screening device to recover the buoyant flotation media, such as a vibratory separator, centrifugal screener, or a cross-flow sieve. The screens used are sized to selectively remove the buoyant flotation particles. Other separation devices, such as centrifuges, hydrocyclones, or fluidized bed classifiers, may also be used. The separated sludge is removed from buoyant media recovery unit 50 through a separated sludge line 52. The separated buoyant flotation particles are removed from buoyant media recovery unit 50 through a buoyant flotation particle recycling line 54 and recycled into flocculation chamber 20.

Having described the currently preferred embodiment of the present invention, it is to be understood that the invention may be otherwise embodied within the scope of the appended claims. For example, the modular

tanks 10, 20 and 30 in Fig. 1 with pipe connections 14, 24 may be replaced by a single large tank (not shown) having appropriate over-weir and under-weir devices to define separate chambers which are fluidly connected in the same general manner as shown in Fig. 1.

WE CLAIM:

1. A process for separating suspended material from a fluid, comprising:

a) adding at least one coagulant and/or at least one flocculant to said fluid to form a mixed fluid;

5 b) adding buoyant media to the mixed fluid;

c) directing the mixed fluid to a flotation chamber and separating the suspended material and buoyant media from the mixed fluid by flotation, resulting in floating sludge being formed in an upper portion of the flotation chamber and clarified fluid formed in a lower portion of the flotation chamber;

d) removing the floating sludge from the flotation chamber; and

10 e) removing clarified fluid from the lower portion of the flotation chamber.

15 2. The process of claim 1 in which a portion of the clarified fluid is recycled to the flotation chamber.

3. The process of claim 1 in which at least a portion of the buoyant media is removed from the floating sludge and is recycled for reuse in the process.

4. The process of claim 1 in which the buoyant media are finely divided solids with a specific gravity less than 1.0.

5. The process of claim 1 in which the buoyant media are solids provided with internal voids.

6. The process of claim 1 additionally comprising introducing a gas to the mixed fluid in a lower portion of the flotation chamber in step c).

7. The process of claim 6 wherein the gas is dissolved air.

~~8.~~ A process for clarifying fluid containing suspended material, comprising:

- a) adding a coagulant and a flocculant to fluid to form a mixed fluid;
- 5 b) adding buoyant media to the mixed fluid;
- c) directing the mixed fluid to a lower portion of a flotation chamber;
- d) separating the suspended material, coagulant, flocculant and buoyant media from the mixed fluid by flotation;
- 10 e) removing the floating sludge from an upper portion of the flotation chamber;
- f) removing at least a portion of the buoyant media from the floating sludge;
- 15 g) recycling at least a portion of the buoyant media to the process in step b) above; and
- h) removing clarified fluid from the lower portion of the flotation chamber.

9. The process of claim 8 in which the buoyant media are finely divided solids with a specific gravity less than 1.0.

10. The process of claim 8 in which the buoyant media are solids provided with internal voids.

11. The process of claim 8 including in step c) the further step of passing the mixed fluid along an upwardly directed baffle in the flotation chamber.

*Def. 91*  
~~12. A system for fluid clarification comprising:~~  
~~a mixing chamber;~~  
~~a flocculation chamber in fluid communication~~  
~~with the mixing chamber;~~

~~a flotation chamber in fluid communication with the flocculation chamber; and~~

~~a buoyant media recovery unit in fluid communication with the flotation chamber and with the flocculation chamber.~~

13. The system of claim 12 further comprising a flotation assistance device in fluid communication with the flotation chamber.

14. The system of claim 12 in which the flotation chamber contains lamella plates.

15. The system of claim 12 in which the flotation chamber contains tubes.

16. The system of claim 12 including a baffle in the flotation chamber to direct entering mixed fluid upward.

17. The system of claim 12 in which the flotation chamber contains immersed membranes.

*Add A2*

**BUOYANT MEDIA FLOTATION**  
**ABSTRACT OF THE DISCLOSURE**

5 A clarification system for fluids in which particles are separated from the fluid by flotation and in which the buoyant media inducing the flotation is recycled. Flotation can be assisted by a flotation assistance device, such as dissolved air flotation.

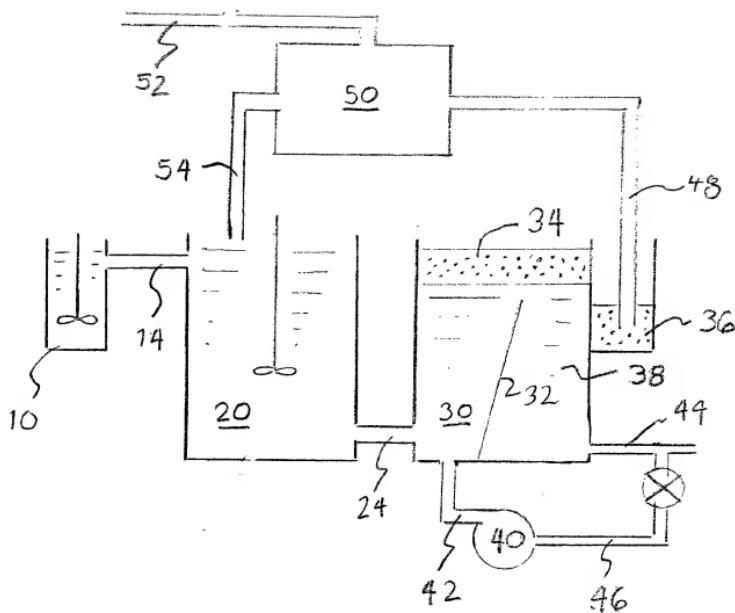


Fig. 1

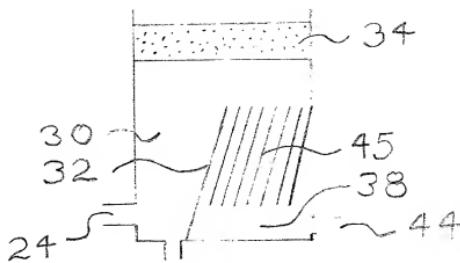


Fig. 2

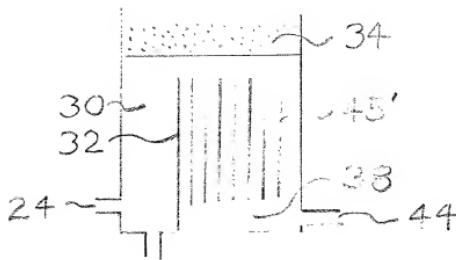


Fig. 3

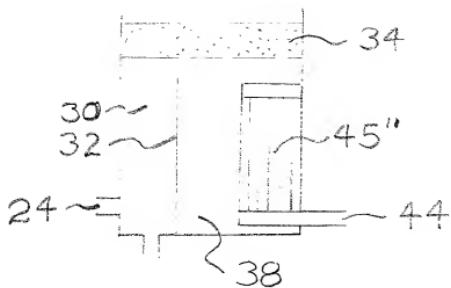


Fig. 4

DECLARATION AND POWER OF ATTORNEY

We, Andrew Eades and Jeffrey Penno, declare:

We are citizens of Great Britain and Canada residing in McCandless Township, County of Allegheny, Commonwealth of Pennsylvania and Ross Township, County of Allegheny, and Commonwealth of Pennsylvania, whose post-office addresses are 9246 Marymont Drive, Pittsburgh, Pennsylvania 15237 and 334 Bascom Avenue, Apt. 206, Pittsburgh, Pennsylvania 15214, respectively.

We believe ourselves to be the original, first and joint inventors of the improvement in "Buoyant Media Flotation" described and claimed in the specification filed concurrently herewith.

We have reviewed and understand the contents of the specification, including the claims.

We do not know and do not believe that the same was ever known or used in the United States before our invention thereof; or patented or described in any printed publication in any country before our invention thereof or more than one year prior to this application; or in public use or on sale in the United States more than one year prior to this application.

Said invention has not been patented or been made the subject of an inventor's certificate in any country foreign to the United States on an application filed by us or our legal representatives or assigns more than twelve months prior to this application.

We acknowledge our duty to disclose information of which we are aware which is material to the patentability of this application in accordance with Title 37, Code of Federal Regulations, §1.56(a).

No application for patent or inventor's certificate thereon has been filed by us or our legal representatives or assigns in any country foreign to the United States.

We declare further that all statements made herein of our own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code and that such willful false statements may jeopardize the validity of the application or any patent issuing thereon.

We hereby appoint William H. Logsdon, Registration No. 22,132; Russell D. Orkin, Registration No. 25,363; David C. Hanson, Registration No. 23,024; Richard L. Byrne, Registration No. 28,498; Frederick B. Ziesenhein, Registration No. 19,438; Kent E. Baldauf, Registration No. 25,826; Barbara E. Johnson, Registration No. 31,198; Paul M. Reznick, Registration No.

33,059; John W. McIlvaine, Registration No. 34,219; Michael I. Shamos, Registration No. 30,424; Blynn L. Shideler, Registration No. 35,034; Julie W. Meder, Registration No. 36,216; Lester N. Fortney, Registration No. 38,141; Randall A. Notzen, Registration No. 36,882; Jesse A. Hirshman, Registration No. 40,016; James G. Porcelli, Registration No. 33,757; Kent E. Baldauf, Jr., Registration No. 36,082; Christian E. Schuster, Registration No. 43,908; Deborah M. Altman, Registration No. 42,259; Dean E. Geibel, Registration No. 42,570; Thomas J. Clinton, Registration No. 40,561; and Nathan J. Prepelka, Registration No. 43,016, whose post-office address is 700 Koppers Building, 436 Seventh Avenue, Pittsburgh, Pennsylvania 15219-1818, Telephone No. 412-471-8815, our attorneys with full power of substitution and revocation, to prosecute this application and to transact all business in the Patent and Trademark Office connected therewith, to amend the specification, to appeal in case of rejection, as they may deem advisable, to receive the patent when granted and generally to do all matters and things needful in the premises, as fully and to all intents and purposes as we could do.

All correspondence and telephone calls should be addressed to John W. McIlvaine.

We hereby subscribe our names to the foregoing specification and claims, declaration and power of attorney.

Date 3rd February 2000 Inventor Andrew Eades  
Andrew Eades

Date 3rd February 2000 Inventor Jeff Penno  
Jeffrey Penno